

ENTHALPY VARIATION OF THE NINE SOLID PHASES OF THE BINARY MOLECULAR ALLOYS (*n*-TRICOSANE:*n*-PENTACOSANE) VS. TEMPERATURE

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Abstract

The enthalpy variations of pure *n*-tricosane (*n*-C₂₃H₄₈), pure *n*-pentacosane (*n*-C₂₅H₅₂) and sixteen binary mixtures were determined from 282 to 360 K. The differential enthalpy analyses were carried out on the pure components, on the four terminal solid solutions, denoted $\beta_0(\text{C}_{23})$, $\beta'_0(\text{C}_{23})$, $\beta_0(\text{C}_{25})$, $\beta'_0(\text{C}_{25})$ and on the three intermediate phases, called β'_1 , β_1 , β'_2 of the binary system (C₂₃:C₂₅) using a calorimeter of the Tian Calvet type. These variations can be represented by an analytical expression, which is derived from Einstein's model. The two Rotator phases β -RI and α -RII were also studied.

Keywords: binary mixtures, enthalpy variations, Einstein's solid model, *n*-pentacosane, *n*-tricosane

Introduction

An estimate of the crystallization point of solid *n* alkanes (hereafter denoted by C_{*n*}) in paraffinic petroleum or middle-distillate fuels is possible only when the thermodynamic properties of the pure components and their respective mixtures are known. In our laboratory joint studies by calorimetry and X-ray diffraction are carried out currently on the liquid/solid and solid/solid equilibria occurring in pure C_{*n*} (17 < *n* < 27) [1], in solution with ethylbenzene [2, 3] and in their respective binary mixtures [4–17]. These studies allowed to determine:

i) the binary phase diagrams of C₂₂:C₂₄ [5, 8], C₂₄:C₂₆ [9, 10], C₂₃:C₂₄ [12], C₂₁:C₂₃ [13, 14] and C₂₃:C₂₅ [15, 16].

ii) the general rules of the thermodynamic and structural behaviour of consecutive [even:even numbered], [even:odd-numbered] and [odd:odd-numbered] *n*-alkane binary mixtures [17].

As for the C₂₄:C₂₆ system [18], the aim of this work is to present the differential enthalpimetric analyses carried out on the solid phases which have been observed in the C₂₃:C₂₅ mixtures [15, 16]. The phase diagram [16] shows the existence of nine solid solution ranges:

i) at low temperature, four terminal solid solutions, denoted $\beta_0(\text{C}_{23})$, $\beta'_0(\text{C}_{23})$, $\beta'_0(\text{C}_{25})$ and $\beta_0(\text{C}_{25})$ and three orthorhombic intermediate solutions: two isostructural phases called β'_1 and β''_1 on both sides of the phase β'_1 .

ii) when the temperature increases, all these phases undergo the same solid/solid transitions as the pure C_{23} and C_{25} , except the δ transition, with appearance of the β phase (Fmmm) which is a second order transition with the Rotator RI state, and just below the solidus line the Rotator phase α -RII ($R\bar{3}m$).

The enthalpy variations vs. temperature are given for the different solid phases. Then data concerning the low temperature phases are treated using a function derived from the Einstein solid model.

Experimental

Measurement principle

The enthalpy measurements were performed with a differential scanning calorimeter of the TIAN-CALVET type [19], a DSC 111 manufactured by SETARAM, using a discontinuous mode of temperature programming.

The calorimeter principle has been described before [18, 20]. It is based on the measurement of the difference of heat Q exchanged between two cells and the calorimeter block during a temperature jump from T_1 to T_2 . On the one hand, the calorimeter asymmetry term Q_D is determined by a blank experiment, in which only the sample support is placed in the measurement cell. On the other hand, the sample is put in its support to measure the overall heat Q_o . The sample contribution Q_s corresponds to the difference between the measurement Q_o and blank Q_D values: $Q_s = Q_o - Q_D$. For each temperature jump j , the molar enthalpy variation is:

$$H(T_2) - H(T_1) = \frac{M}{m}(Q_s)_j$$

where M and m are the molar mass and the mass of the sample, respectively.

The molar enthalpy of sample heating at temperature T , referred to 282K, is:

$$H(T) - H(282) = \sum_j \frac{M}{m}(Q_s)_j$$

where $H(T)$ and $H(282)$ are the enthalpies at T and 282 K, respectively.

The calibration of the apparatus was performed with the help of the thermodynamic data of alumina reported by the N.B.S. Table [21]. The reproductibility and the precision of the enthalpy measurement were determined by using C_{26} for which the experimental enthalpy was compared to that in the literature [22]. The relative standard deviations is about 2% [18].

Operating conditions

The measurements were carried out with a discontinuous programming of the temperature vs. time:

– the rising temperature period was set at 200 s and corresponded to 1 or 0.5 K, depending on the temperature range.

– the temperature level duration depends on a computer test, checking that the calorimeter signal returned to constant value, corresponding to a steady state.

The measurements were carried out in two steps, for both blank and sample.

– from 282 K to 310 K, with a temperature rate of 18 K h^{-1} , giving a temperature jump of 1 K.

– from 300 to 310 K, with a temperature rate of 9 K h^{-1} , giving a temperature jump of 0.5 K.

These two series of measurements overlap over 10 K; no significant differences between the operating conditions were observed.

Sample preparation

The *n*-alkanes C_{23} and C_{25} were obtained from Aldrich Chemical Company and had a stated purity of 99% for C_{25} and over 99% for C_{23} , as determined by gas chromatography and mass spectroscopy. The mixtures were prepared by mixing together appropriate proportions of C_{23} and C_{25} . The samples were obtained by melting, thorough mixing and quenching in a crystallizing dish within a Dewar vessel containing liquid air. Such a rapid cooling ensured a uniform steric concentration of each component in the solid state.

Experimental results

Variation of the enthalpy vs. temperature

The calorimetric measurements were made on pure C_{23} and C_{25} and 16 binary mixtures, covering the whole range of concentrations. The results are presented in Tables 1 to 9. Figure 1 represents the curve of the enthalpy for pure C_{25} and the mixture containing 30 mol% of C_{25} .

Representation of the variations of enthalpy for low temperature phases

We propose to represent the binary system with the help of the Einstein model. Such a binary system behaves like a monoatomic solid of N atoms, having $3N$ independent vibrations, which are harmonic and have the same frequency. This frequency corresponds to a typical temperature θ , called Einstein's

Table 1 Variations of the enthalpy vs. temperature

T/K	$C_{23}: 0 \text{ mol\% } C_{25}$ $H^{282.8}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{23}: 0.3 \text{ mol\% } C_{25}$ $H^{282.8}(T)/J \text{ mol}^{-1}$	Phase
282.8	0		282.8	0	
283.8	547		283.8	605	
284.8	1210		284.8	1211	
285.9	1676		285.9	1619	
286.9	2491		286.8	2411	
287.9	3090		287.8	3025	
288.9	3715		288.9	3646	
289.9	4341		289.9	4274	
290.9	4967		290.9	4885	
292.0	5610		292.0	5500	
293.0	6316	$\beta_0(C_{23})$	293.0	6131	$\beta_0(C_{23})$
294.0	6944		294.0	6766	
295.0	7572		295.0	7384	
296.0	8225		296.0	8026	
297.0	8894		297.0	8681	
298.1	9499		298.1	9314	
299.1	10186		299.1	9950	
300.1	10876		300.1	10613	
301.1	11562		301.1	11281	
302.1	12208		302.1	11919	
303.1	12881		303.1	12579	
304.1	13575		304.1	13241	
304.9	14262		304.9	13907	
305.4	14954		305.4	14569	
305.9	15058		305.9	14332	
306.5	15440		306.4	14701	
307.0	15846		306.9	15095	
307.5	16251		307.4	15498	
308.0	16656		308.0	15907	
308.5	17063		308.3	16350	
309.1	17502	$\beta'_0(C_{23})$	309.0	16784	$\beta'_0(C_{23})$
309.6	17924		309.5	17248	
310.1	18358		310.0	17675	
310.8	18812		310.5	18102	
311.1	19324		311.0	18549	
311.8	19880		311.8	19019	
312.2	20419		312.1	19681	
312.7	20982		312.6	20140	
313.2	20519		313.1	20642	
313.7	41769		313.6	30562	
314.2	42942		314.1	40983	
314.8	44178		314.7	42211	
315.3	45510		315.2	43333	
315.8	46827	β -RI	315.7	44420	β -RI
316.3	47895		316.2	45372	
316.8	48686		316.7	46247	
317.4	49016		317.2	47097	
317.9	50405		317.7	47921	
318.4	51587		318.3	48675	α -RII
318.9	52401		318.8	49655	
319.4	53340	α -RII	319.3	50568	
319.9	54000		319.8	50949	
320.5	83772		320.3	62832	
321.0	102749		320.8	86619	
321.5	103239		321.3	100351	
322.0	103729		321.8	100797	
322.5	104208		322.4	101178	
323.1	104710		322.9	101611	
323.6	105211		323.4	102032	
324.1	105708		323.9	102446	
324.6	106221		324.4	102854	
325.1	106717		324.9	103290	
325.6	107222		325.5	103676	
326.2	107724		326.0	104090	
326.7	108237		326.5	104514	
327.2	108744		327.0	104940	
327.7	109253		327.5	105382	L
328.2	109759		328.0	105798	
328.8	110256	L	328.6	106210	
329.1	110789		329.1	106692	
329.6	111271		329.6	107050	
330.3	111789		330.1	107487	
330.8	112303		330.6	107913	
331.4	112811		331.1	108331	
331.9	113329		331.6	108790	
332.4	113846		332.2	109207	
332.9	114396		332.7	109642	
333.4	114872		333.2	110094	
333.9	115381		333.7	110529	
334.5	115890		334.2	110964	
335.0	116408		334.7	111412	
335.5	116926		335.2	111862	
336.0	117437		335.8	112299	
336.4	117944		336.3	112733	
337.1	118455		336.8	113175	
337.6	118964		337.3	113604	
338.1	119478		337.8	114035	
338.6	119987		338.3	114484	
339.1	120496		338.8	114942	
339.6	121025		339.4	115348	
340.2	121547		339.8	115789	
			340.4	116228	

T : temperature in K; $H^{282.8}(T)$: measured enthalpy, with $T=282.8$ K as reference, in joule per mole;

$\beta_0(C_{23})$: orthorhombic primary solid solution; $\beta'_0(C_{23})$: orthorhombic primary solid solution;

β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L: liquid phase

Table 2 Variations of the enthalpy vs. temperature

T/K	$C_{22}: 0.5 \text{ mol}\% C_{22}$ $H^{282.8}(T)/\text{J mol}^{-1}$	Phase	T/K	$C_{23}: 1.5 \text{ mol}\% C_{23}$ $H^{282.8}(T)/\text{J mol}^{-1}$	Phase
282.8	0		282.8	0	
283.8	865		283.8	582	
284.8	1315		284.8	1188	
285.9	1972		285.9	1838	
286.9	2822		286.9	2455	
287.9	3298		287.9	3160	
288.9	3955		288.9	3855	
289.9	4900		289.9	4430	
290.9	5214		290.9	5083	
292.0	5898	$\beta_0(C_{23})$	292.0	5731	$\beta'_0(C_{23})$
293.0	6513		293.0	6380	
294.0	7187		294.0	7078	
295.0	7824		295.0	7725	
296.0	8485		296.0	8348	
297.0	9103		297.0	8995	
298.1	9724		298.1	9631	
299.1	10374		299.1	10305	
300.1	11037		300.1	10980	
301.1	11883		301.1	11684	
302.1	12848		302.1	12354	
303.1	13013		303.1	13049	
304.1	13683		304.1	13755	
304.9	14042		304.9	14197	
305.4	14364		305.4	14637	
305.9	14719		305.9	15243	
306.4	15052		306.4	16084	
306.9	15373		307.0	16860	
307.4	15698		307.5	17422	
308.0	16030		308.0	17887	
308.5	16378	$\beta'_0(C_{23})$	308.5	18314	β''_1
309.0	16658		309.0	18724	
309.5	17052		309.8	19147	
310.0	17404		310.1	19584	
310.5	17781		310.8	20105	
311.0	18183		311.1	20607	
311.8	18457		311.8	20959	
312.1	18918		312.2	21601	
312.8	35942		312.7	38587	
313.1	36582		313.2	38880	
313.8	35518		313.7	40617	
314.1	40525		314.2	41854	
314.7	41878		314.7	42821	$\beta\text{-RI}$
315.2	42780		315.3	43884	
315.7	43771	$\beta\text{-RI}$	315.8	44792	
316.2	44719		316.3	45640	
316.7	45569		316.8	46370	
317.2	46241		317.3	47100	
317.7	47088		317.8	47850	
318.3	47986		318.4	48588	
318.8	48851		318.9	49329	$\alpha\text{-RII}$
319.3	49448	$\alpha\text{-RII}$	319.4	50224	
319.8	50882		319.9	51223	
320.3	52853		320.5	101048	
320.8	97822		321.0	101440	
321.3	97970		321.5	101820	
321.8	98295		322.0	102210	
322.4	98817		322.5	102680	
322.9	99831		323.1	102980	
323.4	996249		323.6	103370	
323.9	99071		324.1	103787	
324.4	99689		324.6	104205	
324.9	100218		325.1	104635	
325.5	100830		325.7	105042	
326.0	100858		326.2	105457	
326.6	101181		326.7	105859	
327.0	101811		327.2	106281	
327.5	101839		327.7	106689	
328.0	102173		328.3	107142	
328.6	102499		328.8	107595	L
329.1	102825		329.3	107977	
329.7	103103		329.8	108374	
330.1	103478		330.3	108772	
330.6	103820		330.9	109218	
331.1	104148		331.4	109635	
331.6	104485		331.9	110058	
332.2	104823		332.4	110448	
332.7	105145		332.9	110874	
333.2	105468		333.5	111307	
333.7	105778		334.0	111714	
334.2	106112		334.5	112107	
334.7	106435		335.0	112513	
335.2	106767		335.5	112931	
335.8	107075		336.1	113341	
336.3	107397				
336.8	107709				
337.3	108024				
337.8	108348				
338.3	108687				
338.8	109000				
339.4	109319				
339.8	109639				
340.4	109982				

T : temperature in K; $H^{282.8}(T)$: measured enthalpy, with $T=282.8$ K as reference, in joule per mole; $\beta_0(C_{23})$: orthorhombic primary solid solution; $\beta'_0(C_{23})$: orthorhombic primary solid solution; β''_1 : orthorhombic intermediate solid solution; $\beta\text{-RI}$: orthorhombic rotator phase; $\alpha\text{-RII}$: rhombohedral rotator phase; L : liquid phase

Table 3 Variations of the enthalpy vs. temperature

T/K	$C_{23}: 1.8 \text{ mol\% } C_{25}$ $H^{282.8}(T)/\text{J mol}^{-1}$	Phase	T/K	$C_{23}: 2 \text{ mol\% } C_{25}$ $H^{282.8}(T)/\text{J mol}^{-1}$	Phase
282.8	0		282.8	0	
283.8	648		283.8	644	
284.8	1290		284.8	1270	
285.8	1938		285.8	1907	
286.8	2590		286.8	2556	
287.8	3198		287.8	3181	
288.8	3791		288.8	3825	
289.8	4443	$\beta'_0(C_{23})$	289.8	4479	
290.8	5065		290.8	5112	
291.8	5718		291.8	5771	
293.0	6408		293.0	6460	$\beta'_0(C_{23})$
294.0	7044		294.0	7158	
295.0	7696		295.0	7798	
296.0	8362		296.0	8443	
297.0	9044		297.0	9100	
298.1	9704		298.1	9778	
299.1	10388		299.1	10458	
300.1	11050		300.1	11188	
301.1	11726		301.1	11868	
302.1	12423		302.1	12708	
303.1	13112		303.1	13580	
304.1	13854		304.1	14500	
304.8	14278		304.8	14684	
305.4	14787		305.4	15381	
305.8	15418		305.8	15814	
306.4	16008		306.5	16212	
306.8	16528		307.0	16588	
307.4	17041		307.5	16979	
308.0	17482		308.0	17375	
308.5	17924		308.5	17775	
309.0	18372	β''_1	309.1	18201	β''_1
309.5	18838		309.8	18628	
310.0	19295		310.1	19070	
310.5	19782		310.8	19541	
311.0	20282		311.1	20033	
311.8	20701		311.8	20428	
312.1	20828		312.2	20588	
312.8	21270		312.7	21041	
313.1	20211		313.2	20247	
313.8	20188		313.7	20824	
314.1	40283		314.2	40338	
314.7	41301	$\beta\text{-RI}$	314.8	41417	
316.2	42280		315.3	42430	$\beta\text{-RI}$
316.7	43222		315.8	43418	
318.2	44119		316.3	44314	
318.7	44807		316.8	45126	
317.2	48244		317.3	45848	
317.7	48510		317.8	46862	
318.3	48528		318.4	47575	
318.8	48688		318.9	48211	
319.3	47710	$\alpha\text{-RII}$	319.4	48883	$\alpha\text{-RII}$
319.8	48733		319.9	49731	
320.3	52377		320.6	51822	
320.6	50774		321.0	51867	
321.3	100584		321.5	51088	
321.8	100601		322.0	51455	
322.4	101233		322.5	51738	
322.9	101587		323.1	52215	
323.4	101881		323.6	52801	
323.8	102227		324.1	53673	
324.4	102598		324.6	54338	
324.8	102888		325.1	54974	
325.5	103258		325.6	55623	
326.0	103602		326.2	56285	
326.5	103943		326.7	56964	
327.0	104275	L	327.2	57654	
327.5	104607		327.7	58355	
328.0	104948		328.2	59068	
328.6	105288		328.8	59787	
329.1	105644		329.3	60527	L
329.6	106004		329.8	61288	
330.1	106338		330.3	62068	
330.8	106678		330.8	62864	
331.1	107008		331.5	63672	
331.6	107348		331.9	64481	
332.2	107704		332.4	65300	
332.7	108045		332.9	66122	
333.2	108385		333.4	66967	
333.7	108741		333.9	67827	
334.2	109077		334.6	68699	
334.7	109410		335.0	69588	
335.2	109738		335.6	70493	
335.8	110088		336.0	71412	
336.3	110441		336.5	72344	
336.8	110771		337.1	73288	
337.3	111084		337.6	74244	
337.8	111427		338.1	75212	
338.3	111758		338.6	76193	
338.8	112102		339.1	77188	
339.4	112430		339.6	78194	
339.9	112755		340.2	79212	
340.4	113078		340.7	80243	

T : temperature in K, $H^{282.8}(T)$: measured enthalpy, with $T=282.8$ K as reference, in joule per mole; $\beta'_0(C_{23})$: orthorhombic primary solid solution; β''_1 : orthorhombic intermediate solid solution; $\beta\text{-RI}$: orthorhombic rotator phase; $\alpha\text{-RII}$: rhombohedral rotator phase; L : liquid phase

Table 4 Variations of the enthalpy vs. temperature

<i>T</i> /K	C_{25}^3 3 mol% C_{25}^2 $H^{282.8}(T)/J \text{ mol}^{-1}$	Phase	<i>T</i> /K	C_{25}^4 4 mol% C_{25}^2 $H^{282.8}(T)/J \text{ mol}^{-1}$	Phase
282.8	0		282.8	0	
283.8	657		283.8	830	
284.8	1316		284.8	1281	
285.9	1988		285.9	1938	
286.9	2669		286.9	2600	
287.9	3293		287.9	3219	
288.9	3987		288.9	3859	
289.9	4672		289.9	4524	
290.9	5334		290.9	5200	β''_1
292.0	6026	β''_1	292.0	5883	
293.0	6657		293.0	6580	
294.0	7334		294.0	7231	
295.0	8068		295.0	7919	
296.0	8795		296.0	8605	
297.0	9530		297.0	9297	
298.1	10284		298.1	9987	
299.1	11024		299.1	10705	
300.1	11777		300.1	11420	
301.1	12518		301.1	12154	
302.1	13285		302.1	12870	
303.1	14029		303.1	13638	
304.1	14787		304.1	14418	
304.9	15194		304.9	15204	
305.4	15548		305.9	15532	
305.9	15937		306.5	15825	
306.5	16324		307.0	16323	
307.0	16899		307.5	16748	
307.5	17119		308.0	17205	
308.0	17451		308.4	17600	
308.5	17866		308.0	18198	
309.1	18283		308.8	27405	
309.8	18683		310.1	32757	
310.1	19180		310.8	33370	
310.8	24586		311.1	34374	
311.1	25228		311.8	35109	
311.8	35173		312.2	36042	
312.2	36028		312.7	36822	
312.7	36884		313.2	37681	β -RI
313.2	37720		313.7	38772	
313.7	38729		314.2	39889	
314.2	39752	β -RI	314.7	40998	
314.8	40707		315.3	41492	
315.3	41688		315.8	42242	
315.8	42586		316.3	43005	
316.3	43434		316.8	43894	
316.9	43786		317.3	44379	
317.4	44180		317.8	45182	
317.9	44906		318.4	45987	α -RII
318.4	45717	α -RII	318.8	46953	
318.9	46328		318.4	47778	
318.4	46961		318.9	50186	
318.9	47786		320.4	57888	
320.9	49823		321.0	59097	
321.0	50002		321.5	64528	
321.5	62967		322.0	64646	
322.0	63350		322.5	65182	
322.5	63715		323.0	65498	
323.1	64070		323.6	65841	
323.6	64413		324.1	66187	
324.1	64785		324.6	66497	
324.6	65111		325.1	66803	
325.1	65482		325.6	67088	L
325.6	65818		326.1	67432	
326.2	66182		326.7	67770	
326.7	66563	L	327.2	68060	
327.2	66900		327.7	68358	
327.7	67242		328.2	68725	
328.2	67582		328.7	69035	
328.8	67979		329.3	69337	
329.3	68331		329.8	69678	
329.8	68694		330.3	69988	
330.3	69059		330.8	70313	
330.8	69432		331.3	70618	
331.3	69837		331.8	70937	
331.8	70233		332.4	71289	
332.4	70618		332.9	71583	
332.9	71028		333.4	71906	
333.4	71450		333.9	72203	
333.9	71829		334.4	72525	
334.5	72170		334.9	72825	
335.0	72533		335.5	73147	
335.5	72880		336.0	73487	
336.0	73256		336.5	73863	
336.5	73618		337.0	74180	
337.1	73982		337.5	74427	
337.6	74330		338.1	74740	
338.1	74679		338.6	75050	
338.6	75035		339.1	75351	
339.1	75397		339.6	75688	
339.6	75719		340.1	75965	
340.2	76089				
340.7	76469				

T: temperature in K; $H^{282.8}(T)$: measured enthalpy, with $T=282.8$ K as reference, in joule per mole; β''_1 : orthorhombic intermediate solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L : liquid phase

Table 5 Variations of the enthalpy vs. temperature

T/K	$C_{25}: 25 \text{ mol\% } C_{25}$ $H^{282.8}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{25}: 30 \text{ mol\% } C_{25}$ $H^{282.8}(T)/J \text{ mol}^{-1}$	Phase
282.8	0		282.8	0	
283.8	862		283.8	866	
284.8	1362		284.8	1308	
285.8	2061		285.8	1976	
286.8	2751		286.8	2658	
287.8	3438		287.8	3367	
288.8	4124		288.8	4079	
289.8	4813		289.8	4786	
290.8	5515		290.8	5524	
292.0	6236		292.0	6247	
293.0	6963	β^*	293.0	6988	
294.0	7689		294.0	7721	β^*
295.0	8418		295.0	8458	
296.0	9158		296.0	9208	
297.0	9888		297.0	9943	
298.1	10644		298.1	10686	
299.1	11417		299.1	11481	
300.1	12188		300.1	12228	
301.1	12866		301.1	13014	
302.1	13814		302.1	13623	
303.1	14650		303.1	14630	
304.1	15444		304.1	15478	
304.9	15883		304.9	15855	
305.4	16304		305.4	16355	
305.9	16769		305.9	16847	
306.5	17557		306.4	20168	
307.0	28038		308.9	27305	
307.4	28368		307.4	28602	
308.0	29807		308.0	29881	
308.5	30327		308.5	30431	
309.1	31081		309.0	31219	
309.8	31825		309.5	32066	
310.1	32585	β -RI	310.0	32810	
310.6	33358		310.6	33788	
311.1	34138		311.1	34688	β -RI
311.8	34920		311.8	35617	
312.2	35749		312.1	36523	
312.7	36547		312.8	37455	
313.2	37378		313.1	38350	
314.7	38168		313.7	39256	
314.2	38977		314.2	40155	
314.6	39738		314.7	40870	
315.5	40429		315.2	41704	
315.8	41080		315.7	42415	
316.3	41704		316.3	43123	
316.8	42289		316.8	43805	
317.4	42919		317.3	44578	
317.9	43473		317.8	45280	
318.4	44013	α -RII	318.3	45885	
318.9	44582		318.8	46744	α -RII
319.4	45203		319.4	47616	
319.8	45798		319.9	48687	
320.5	46478		320.4	50094	
321.0	47451		320.9	52332	
321.5	51135		321.4	37634	
322.0	83511		322.0	78015	
322.5	82018		322.5	88738	
323.1	82414		323.0	87346	
323.0	82704		323.5	87831	
324.1	83132		324.0	88334	
324.8	83454		324.8	88787	
325.1	83813		325.1	89254	
325.8	84188		325.8	89716	
326.2	84513		326.1	100186	
326.7	84889		326.8	109654	
327.2	85214		327.1	101120	
327.7	85578		327.7	101581	
328.2	85985	L	328.2	102075	
328.5	86324		328.7	102568	L
329.3	86851		329.2	103021	
329.8	87049		329.7	103488	
330.3	87395		330.3	103983	
330.8	87735		330.8	104413	
331.3	88064		331.3	104888	
331.8	88441		331.8	105387	
332.4	88783		332.3	105842	
332.9	89130		332.8	106315	
333.4	89520		333.4	106813	
333.9	89885		333.9	107301	
334.5	100200		334.4	107781	
335.0	100584		334.9	108248	
335.5	100921		335.4	108732	
336.0	101273		336.0	109208	
336.5	101625				
337.1	101983				
337.8	102303				
338.1	102650				
338.8	103020				
339.1	103388				
339.8	103890				
340.2	104040				

T : temperature in K; $H^{282.8}(T)$: measured enthalpy, with $T=282.8$ K as reference, in joule per mole; β^* : orthorhombic intermediate solid solution; β RI: orthorhombic rotator phase; α RII: rhombohedral rotator phase; L: liquid phase

Table 6 Variations of the enthalpy vs. temperature

<i>T</i> /K	$C_{25}; 40 \text{ mol\% } C_{25}$ $H^{282.8}(T)/\text{J mol}^{-1}$	Phase	<i>T</i> /K	$C_{25}; 53 \text{ mol\% } C_{25}$ $H^{282.8}(T)/\text{J mol}^{-1}$	Phase
282.8	0		282.8	0	
283.8	697		283.8	754	
284.8	1423		284.8	1413	
285.8	2108		285.8	2117	
286.8	2789		286.8	2838	
287.8	3588		287.8	3543	
288.8	4289		288.8	4281	
289.8	5028		289.8	4956	
289.9	5742		289.9	5686	β'
292.0	6438		292.0	6418	
293.0	7157	β'	293.0	7127	
294.0	7898		294.0	7846	
295.0	8625		295.0	8604	
296.0	9359		296.0	9338	
297.0	10121		297.0	10085	
298.1	10981		298.1	10910	
298.1	11871		298.1	11894	
300.1	12458		300.1	12379	
301.1	13221		301.1	13158	
302.1	14004		302.1	13960	
303.1	14784		303.1	14784	
304.1	15565		304.1	15629	
304.8	15985		304.8	16115	
305.4	16403		305.4	16633	
305.9	16872		305.9	17164	
306.4	17414		306.5	17728	
308.8	18483		307.0	18551	
307.4	24865		307.5	24083	
308.0	26222		308.0	26590	
308.5	30314		308.5	29999	
309.0	31086		309.1	30300	
309.5	31834		309.6	31621	
310.0	32613		310.1	32464	
310.5	33423		310.6	33303	
311.0	34257		311.1	34141	
311.6	35044		311.6	35011	
312.1	35850	β -RI	312.2	35917	
312.8	36754		312.7	36826	
313.1	37648		313.2	37778	β -RI
313.6	38537		313.7	38712	
314.1	39434		314.2	39641	
314.7	40287		314.8	40516	
315.2	41096		315.3	41330	
315.7	41845		315.8	42103	
316.2	42625		316.3	42835	
316.7	43162		316.8	43532	
317.2	43853		317.4	44272	
317.7	44440		317.9	44968	
318.3	45057		318.4	45549	
318.8	45829	α -RII	318.9	46184	
319.3	46231		319.4	46828	
319.8	46867		319.9	47482	α -RII
320.3	47919		320.0	48140	
320.8	48171		321.0	48814	
321.3	48841		321.5	49534	
321.8	50588		322.0	50482	
322.4	62168		322.5	60502	
322.9	83980		323.1	81883	
323.4	84883		323.6	87910	
323.9	86060		324.1	97758	
324.4	96322		324.6	98225	
324.9	98988		325.1	98676	
325.5	100397		325.6	99151	
326.0	100805		326.2	99612	
326.5	101243		326.7	100060	
327.0	101678		327.2	100509	
327.5	102094	L	327.7	101059	L
328.0	102509		328.2	101518	
328.8	102829		328.8	102004	
329.1	103364		329.3	102465	
329.6	103798		329.8	102940	
330.1	104219		330.3	103423	
330.6	104683		330.8	103908	
331.1	105100		331.3	104384	
331.6	105538		331.9	104861	
332.2	105985		332.4	105342	
332.7	106384		332.9	105814	
333.2	106908		333.4	106288	
333.7	107223		333.9	106778	
334.2	107699		334.5	107262	
334.7	108116		335.0	107733	
335.2	108587		335.5	108207	
335.8	108963		336.0	108680	
336.3	109433		336.6	109166	
336.8	109893		337.1	109647	
337.3	110333		337.6	110132	
337.8	110765		338.1	110612	
338.3	111202		338.6	111097	
338.8	111645		339.1	111584	
339.4	112085		339.6	112074	
339.9	112521		340.2	112552	
340.4	112960		340.7	113028	
			341.2	113488	

T: temperature in K; $H^{282.8}(T)$: measured enthalpy, with $T=282.8$ K as reference, in joule per mole; β' : orthorhombic intermediate solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L : liquid phase

Table 7 Variations of the enthalpy vs. temperature

T/K	$C_{25}: 80 \text{ mol\% } C_{25}$ $H^{282.8}(T)/\text{J mol}^{-1}$	Phase	T/K	$C_{25}: 84 \text{ mol\% } C_{25}$ $H^{282.8}(T)/\text{J mol}^{-1}$	Phase
282.8	0		282.8	0	
283.8	962		283.8	882	
284.8	1330		284.8	1343	
285.8	1673		285.8	2023	
286.8	2073		286.8	2764	
287.8	2478		287.8	3488	
288.8	2878		288.8	4191	
289.8	3278		289.8	4871	
290.8	3678		290.8	5543	
291.8	4078		291.8	6208	β''_2
292.8	4478		292.8	6878	
293.8	4878		293.8	7548	
294.8	5278		294.8	8218	
295.8	5678		295.8	8888	
296.8	6078		296.8	9558	
297.8	6478		297.8	10228	
298.8	6878		298.8	10898	
299.8	7278		299.8	11568	
300.8	7678		300.8	12238	
301.8	8078		301.8	12908	
302.8	8478		302.8	13578	
303.8	8878		303.8	14248	
304.8	9278		304.8	14918	
305.8	9678		305.8	15588	
306.8	10078		306.8	16258	
307.8	10478		307.8	16928	
308.8	10878		308.8	17598	
309.8	11278		309.8	18268	
310.8	11678		310.8	18938	
311.8	12078		311.8	19608	
312.8	12478		312.8	20278	
313.8	12878		313.8	20948	
314.8	13278		314.8	21618	
315.8	13678		315.8	22288	
316.8	14078		316.8	22958	
317.8	14478		317.8	23628	
318.8	14878		318.8	24298	
319.8	15278		319.8	24968	
320.8	15678		320.8	25638	
321.8	16078		321.8	26308	
322.8	16478		322.8	26978	
323.8	16878		323.8	27648	
324.8	17278		324.8	28318	
325.8	17678		325.8	28988	
326.8	18078		326.8	29658	
327.8	18478		327.8	30328	
328.8	18878		328.8	30998	
329.8	19278		329.8	31668	
330.8	19678		330.8	32338	
331.8	20078		331.8	33008	
332.8	20478		332.8	33678	
333.8	20878		333.8	34348	
334.8	21278		334.8	35018	
335.8	21678		335.8	35688	
336.8	22078		336.8	36358	
337.8	22478		337.8	37028	
338.8	22878		338.8	37698	
339.8	23278		339.8	38368	
340.8	23678		340.8	39038	
341.8	24078		341.8	39708	
342.8	24478		342.8	40378	
343.8	24878		343.8	41048	
344.8	25278		344.8	41718	
345.8	25678		345.8	42388	
346.8	26078		346.8	43058	
347.8	26478		347.8	43728	
348.8	26878		348.8	44398	
349.8	27278		349.8	45068	
350.8	27678		350.8	45738	
351.8	28078		351.8	46408	
352.8	28478		352.8	47078	
353.8	28878		353.8	47748	
354.8	29278		354.8	48418	
355.8	29678		355.8	49088	
356.8	30078		356.8	49758	
357.8	30478		357.8	50428	
358.8	30878		358.8	51098	
359.8	31278		359.8	51768	
360.8	31678		360.8	52438	
361.8	32078		361.8	53108	
362.8	32478		362.8	53778	
363.8	32878		363.8	54448	
364.8	33278		364.8	55118	
365.8	33678		365.8	55788	
366.8	34078		366.8	56458	
367.8	34478		367.8	57128	
368.8	34878		368.8	57798	
369.8	35278		369.8	58468	
370.8	35678		370.8	59138	
371.8	36078		371.8	59808	
372.8	36478		372.8	60478	
373.8	36878		373.8	61148	
374.8	37278		374.8	61818	
375.8	37678		375.8	62488	
376.8	38078		376.8	63158	
377.8	38478		377.8	63828	
378.8	38878		378.8	64498	
379.8	39278		379.8	65168	
380.8	39678		380.8	65838	
381.8	40078		381.8	66508	
382.8	40478		382.8	67178	
383.8	40878		383.8	67848	
384.8	41278		384.8	68518	
385.8	41678		385.8	69188	
386.8	42078		386.8	69858	
387.8	42478		387.8	70528	
388.8	42878		388.8	71198	
389.8	43278		389.8	71868	
390.8	43678		390.8	72538	
391.8	44078		391.8	73208	
392.8	44478		392.8	73878	
393.8	44878		393.8	74548	
394.8	45278		394.8	75218	
395.8	45678		395.8	75888	
396.8	46078		396.8	76558	
397.8	46478		397.8	77228	
398.8	46878		398.8	77898	
399.8	47278		399.8	78568	
400.8	47678		400.8	79238	
401.8	48078		401.8	79908	
402.8	48478		402.8	80578	
403.8	48878		403.8	81248	
404.8	49278		404.8	81918	
405.8	49678		405.8	82588	
406.8	50078		406.8	83258	
407.8	50478		407.8	83928	
408.8	50878		408.8	84598	
409.8	51278		409.8	85268	
410.8	51678		410.8	85938	
411.8	52078		411.8	86608	
412.8	52478		412.8	87278	
413.8	52878		413.8	87948	
414.8	53278		414.8	88618	
415.8	53678		415.8	89288	
416.8	54078		416.8	89958	
417.8	54478		417.8	90628	
418.8	54878		418.8	91298	
419.8	55278		419.8	91968	
420.8	55678		420.8	92638	
421.8	56078		421.8	93308	
422.8	56478		422.8	93978	
423.8	56878		423.8	94648	
424.8	57278		424.8	95318	
425.8	57678		425.8	95988	
426.8	58078		426.8	96658	
427.8	58478		427.8	97328	
428.8	58878		428.8	97998	
429.8	59278		429.8	98668	
430.8	59678		430.8	99338	
431.8	60078		431.8	100008	
432.8	60478		432.8	100678	
433.8	60878		433.8	101348	
434.8	61278		434.8	102018	
435.8	61678		435.8	102688	
436.8	62078		436.8	103358	
437.8	62478		437.8	104028	
438.8	62878		438.8	104698	
439.8	63278		439.8	105368	
440.8	63678		440.8	106038	
441.8	64078		441.8	106708	
442.8	64478		442.8	107378	
443.8	64878		443.8	108048	
444.8	65278		444.8	108718	
445.8	65678		445.8	109388	
446.8	66078		446.8	110058	
447.8	66478		447.8	110728	
448.8	66878		448.8	111398	
449.8	67278		449.8	112068	
450.8	67678		450.8	112738	
451.8	68078		451.8	113408	
452.8	68478		452.8	114078	
453.8	68878		453.8	114748	
454.8	69278		454.8	115418	
455.8	69678		455.8	116088	
456.8	70078		456.8	116758	
457.8	70478		457.8	117428	
458.8	70878		458.8	118098	
459.8	71278		459.8	118768	
460.8	71678		460.8	119438	
461.8	72078		461.8	120108	
462.8	72478		462.8	120778	
463.8	72878		463.8	121448	
464.8	73278		464.8	122118	
465.8	73678		465.8	122788	
466.8	74078		466.8	123458	
467.8	74478		467.8	124128	
468.8	74878		468.8	124798	
469.8	75278		469.8	125468	
470.8	75678		470.8	126138	
471.8	76078		471.8	126808	
472.8	76478		472.8	127478	
473.8	76878		473.8	128148	
474.8	77278		474.8	128818	
475.8	77678		475.8	129488	
476.8	78078		476.8	130158	
477.8	78478		477.8	130828	
478.8	78878		478.8	131498	
479.8	79278		479.8	132168	
480.8	79678		480.8	132838	
481.8	80078		481.8	133508	
482.8	80478		482.8	134178	
483.8	80878		483.8	134848	
484.8	81278		484.8	135518	
485.8	81678		485.8	136188	
486.8	82078		486.8	136858	
487.8	82478		487.8	137528	
488.8	82878		488.8	138198	
489.8	83278		489.8	138868	
490.8	83678		490.8	139538	
491.8	84078		491.8	140208	
492.8	84478		492.8	140878	
493.8	84878		493.8	141548	
494.8	85278		494.8	142218	
495.8	85678		495.8	142888	
496.8	86078		496.8	143558	
497.8	86478		497.8	144228	
498.8	86878		498.8	144898	
499.8	87278		499.8	145568	
500.8	87678		500.8	146238	

T : temperature in K; $H^{282.8}(T)$: measured enthalpy, with $T=282.8$ K as reference, in joule per mole; β'_2 : orthorhombic intermediate solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L: liquid phase

Table 8 Variations of the enthalpy vs. temperature

<i>T</i> /K	C_{25} : 88 mol% C_{27} $H^{282.8}(T)$ /J mol ⁻¹	Phase	<i>T</i> /K	C_{25} : 95 mol% C_{26} $H^{282.8}(T)$ /J mol ⁻¹	Phase
282.8	0		282.8	0	
283.8	711		283.8	653	
284.8	1429		284.8	1309	
285.8	2165		285.8	1978	
286.9	2887		286.9	2525	
287.9	3588		287.9	2886	
288.9	4347		288.9	3321	
289.9	5089		289.9	4007	
290.9	5822	β''_2	290.9	4685	$\beta_0(C_{25})$
292.0	6539		292.0	5313	
293.0	7314		293.0	5898	
294.0	8060		294.0	6532	
295.0	8789		295.0	7342	
296.0	9574		296.0	8040	
297.0	10318		297.0	8720	
298.1	11072		298.1	9409	
299.1	11853		299.1	10104	
300.1	12632		300.1	10839	
301.1	13432		301.1	11583	
302.1	14173		302.1	12311	
303.1	14898		303.1	13072	
304.1	15715		304.1	13837	
304.8	16524		304.8	14733	
305.4	17442		305.4	14808	
305.9	18795		305.9	15073	
306.4	17145		306.4	15518	
306.9	17812		306.9	15824	
307.4	17872		307.4	16379	
308.0	18220		308.0	16847	
308.5	18584		308.5	17353	
309.0	18842		309.0	17828	
309.5	19205		309.5	18334	
310.0	19884		310.0	18839	
310.5	20037		310.5	18398	
311.1	20400		311.1	18777	
311.8	20788		311.8	20278	
312.1	21181		312.1	20752	
312.8	21678		312.8	21190	
313.1	22001		313.1	21623	
313.7	22479		313.7	22053	$\beta'_0(C_{25})$
314.2	23070		314.2	22418	
314.7	23631		314.7	22825	
315.2	24459		315.2	23358	
315.7	25727		315.7	23720	
316.2	26855		316.2	24187	
316.8	34437		316.8	24674	
317.3	40205		317.3	25434	
317.8	44050		317.8	26221	
318.3	48151		318.3	30401	
318.8	48137		318.8	40549	
319.4	48628		319.4	47312	
319.9	47855	β -RI	319.9	48570	
320.4	48990		320.4	48608	
320.9	49991		320.9	50482	β -RI
321.4	49830		321.4	51189	
321.9	50179		321.9	51871	
322.5	50738		322.5	52653	
323.0	51298		323.0	53382	
323.5	51888	α -RII	323.5	53844	
324.0	52450		324.0	54820	α -RII
324.5	53039		324.5	55322	
325.0	53664		325.0	56053	
325.8	55334		325.8	56804	
326.1	62022		326.1	60417	
326.8	102724		326.8	97008	
327.1	103052		327.1	105948	
327.6	103433		327.6	105477	
328.2	103784		328.2	105908	
328.7	104131		328.7	106346	
329.2	104474		329.2	106811	
329.7	104821		329.7	107247	
330.2	105201		330.2	107681	
330.7	105642		330.7	108131	
331.3	105878		331.3	108591	
331.8	106227	L	331.8	109097	
332.3	106581		332.3	109453	
332.8	106943		332.8	109804	
333.3	107279		333.3	110399	
333.8	107830		333.8	110810	L
334.4	107999		334.4	111245	
334.8	108318		334.8	111890	
335.4	108859		335.4	112155	
335.9	108852		335.9	112585	
336.4	109018		336.4	113035	
336.8	109365		336.8	113476	
337.0	109708		337.0	113927	
337.5	108708		337.5	114357	
338.0	110061		338.0	114808	
338.5	110408		338.5	115282	
338.9	110724		338.9	115718	
339.8	111079		339.8	116150	
340.1	111458		340.1	116582	
340.6	111769		340.6	116582	

T: temperature in K; $H^{282.8}(T)$: measured enthalpy, with $T=282.8$ K as reference, in joule per mole; β''_2 : orthorhombic in intermediate solid solution; $\beta'_0(C_{25})$: orthorhombic primary solid solution; $\beta_0(C_{25})$: orthorhombic primary solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; *L*: liquid phase

Table 9 Variations of the enthalpy vs. temperature

T/K	$C_{25}, 97.5 \text{ mol}\% \text{ C}_{25}$ $H^{282.8}(T)/\text{J mol}^{-1}$	Phase	T/K	C_{25} $H^{282.8}(T)/\text{J mol}^{-1}$	Phase
282.8	0		282.8	0	
283.5	722		283.8	832	
284.5	1387		284.8	1288	
285.9	2028		285.9	1818	
289.9	2855		289.9	2542	
287.9	3338		287.9	3203	
288.8	4013		288.9	3883	
289.9	4703		289.9	4548	
290.9	5380		290.9	5207	
282.0	6039		282.0	5866	
293.0	6707	$\beta_0(\text{C}_{25})$	293.0	6549	
294.0	7383		294.0	7212	
295.0	8077		295.0	7873	
298.0	8789		298.0	8560	$\beta_0(\text{C}_{25})$
297.0	8470		297.0	8274	
298.1	10189		298.1	8918	
299.1	10949		299.1	10541	
300.1	11593		300.1	11342	
301.1	12273		301.1	12044	
302.1	12991		302.1	12863	
303.1	13713		303.1	13382	
304.3	14453		304.1	14104	
304.8	14828		305.4	14808	
305.4	15228		305.9	15134	
305.9	15901		308.4	15478	
306.4	15987		308.9	15817	
308.9	18379		307.4	16185	
307.4	19762		306.0	16010	
308.0	17245		308.5	16848	
308.5	17818		308.0	17187	
309.0	18007		308.5	17530	
309.5	18383		310.0	17875	
310.0	18782		310.5	18220	
310.5	19718		311.4	18871	
311.1	19898		311.8	18938	
311.8	20100		312.1	19423	
312.1	20673		312.8	19723	
312.8	21045		313.1	20092	
313.1	21545		313.7	20476	
313.7	22098		314.2	20856	
314.2	22722		314.7	21237	
314.7	23322		315.2	21810	
315.2	24022		315.7	21989	
315.7	24850		316.2	22301	
316.2	25430	$\beta'_0(\text{C}_{25})$	316.8	22742	
316.8	26874		317.4	23171	
317.3	28335		317.8	23508	
317.8	28821		318.3	23818	
318.3	27489		318.8	24353	$\beta'_0(\text{C}_{25})$
318.8	28348		319.4	25129	
319.4	37307		319.9	27443	
319.9	40739		320.4	40280	
320.4	50843		320.9	48989	
320.8	62088		321.4	50128	
321.4	52829		321.9	51154	
321.8	53680		322.5	51995	$\beta\text{-RI}$
322.5	54482		323.0	52834	
323.0	59084	$\beta\text{-RI}$	323.5	53243	
323.5	56731		324.0	53855	$\alpha\text{-RII}$
324.0	56383		324.5	54481	
324.5	57021	$\alpha\text{-RII}$	325.0	55083	
325.0	57705		325.8	55718	
325.8	68489		326.1	56380	
326.1	60130		326.8	57323	
326.8	65589		327.1	111747	
327.1	110147		327.8	113098	
327.8	110591		328.2	113471	
328.2	110689		328.7	113845	
328.7	111478		329.2	114220	
329.2	111849		329.7	114595	
329.7	112276		330.2	114983	
330.2	112898		330.7	115323	
330.7	113128		331.3	115806	
331.3	113558		331.8	116049	
331.8	113898	L	332.3	116414	
332.3	114408		332.8	116782	
332.8	114827		333.3	117152	
333.3	115244		333.8	117522	L
333.8	115899		334.4	117894	
334.4	116138		334.9	118285	
334.9	116464		335.4	118629	
335.4	116989		335.8	118991	
335.9	117424		336.4	119359	
336.4	117851		337.0	119714	
337.0	118300		337.5	120080	
337.5	118738		338.0	120473	
338.0	119182		338.4	120884	
338.5	119625		339.0	121225	
339.0	120082		339.8	121802	
339.8	120490		340.1	121874	
340.1	120819		340.8	122343	

T : temperature in K; $H^{282.8}(T)$: measured enthalpy, with $T=282.8$ K as reference, in joule per mole; $\beta_0(\text{C}_{25})$: orthorhombic primary solid solution; $\beta'_0(\text{C}_{25})$: orthorhombic primary solid solution; $\beta\text{-RI}$: orthorhombic rotator phase; $\alpha\text{-RII}$: rhombohedral rotator phase; L : liquid phase

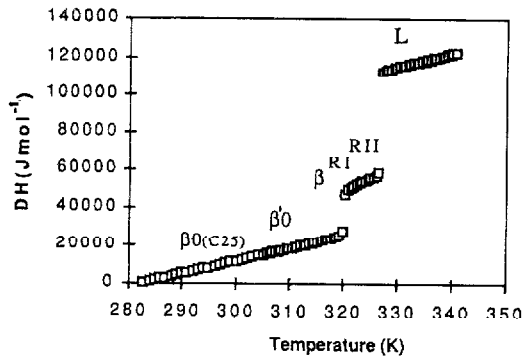


Fig. 1a Enthalpy curve for pure *n*-pentacosane

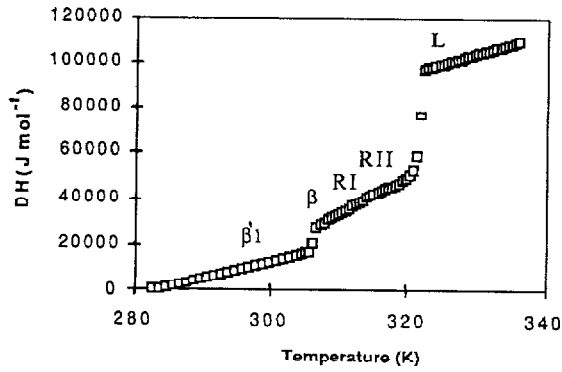


Fig. 1b Enthalpy curve for the mixture containing 30 mol% of *n*-pentacosane

temperature. For each composition, the enthalpy variations can be described by the following expression, derived from the Einstein model:

$$H(T) - H(282) = \frac{3NR\theta}{\exp(\theta/T)} - H_E$$

The parameters N , θ and the integration constant H_E , are optimised using the Rosenbrock method [23], from the temperature and enthalpy data corresponding to $\beta_0(n-C_{23})$, $\beta'_0(n-C_{23})$, β'_1 , β'_1 , β'_2 and $\beta_0(n-C_{25})$ with the error function which is defined by:

$$F(\theta, x) = \sum_{i=1}^n (\Delta H(x)_{\text{exp}} - \Delta H(\theta, x)_{\text{calc}})^2$$

where:

$\Delta H(x)_{\text{exp}}$ is the variation of enthalpy measured for each molar fraction x .
 $\Delta H(\theta, x)_{\text{calc}}$ is the variation of enthalpy calculated for each molar fraction x .
 n is the number of points taken into account for the optimization.

For instance, Table 11 presents the values of the enthalpy variations calculated from the best parameters N, θ and H_E (Table 10), compared to the experimental data for a mixture of 30% molar in C_{25} : the agreement between experimental and calculated values is good; the relative standard deviation is 1.5% as maximum, except for the first value which is always imprecise.

Expressions of the enthalpy $H(T, x)$ as function of the temperature and composition can be defined by the study of the variation of the parameters N and θ vs. composition.

Table 10 Parameters N, θ, H_E vs. composition in $n\text{-}C_{25}H_{52}$

$x/\text{mol}\%$ in $C_{25}H_{52}$	Phase	Temperature domain/K	N	θ/K	$H_E/J\text{ mol}^{-1}$	Error function/ $J\text{ mol}^{-1}$
0	$\beta_0(C_{23})$	282.8–307.2	60.2	981.9	47276	9716
0.3	$\beta_0(C_{23})$	282.8–309.2	60.4	999.3	45268	19073
0.5	$\beta_0(C_{23})$	282.8–306.2	72.4	1096.3	41884	20559
1.5	$\beta'_0(C_{23})$	282.8–306.2	56.9	937.2	50252	33078
2	$\beta'_0(C_{23})$	282.8–302.1	82.2	1145.9	41576	21096
1.8	$\beta'_0(C_{23})$	282.8–305.2	71.7	1076.2	43761	17116
3	β''_1	282.8–308.2	137.3	1385.7	35578	19520
4	β''_1	282.8–307.2	146.1	1428.6	33464	34729
25	β'_1	282.8–305.2	172.9	1477.9	34395	18531
30	β'_1	282.8–305.2	157.2	1429.0	36038	17256
53	β'_1	282.8–306.2	142.9	1379.9	37588	54337
40	β'_1	282.8–307.2	115.3	1269.7	41370	85523
80	β''_2	282.8–308.2	144.9	1391.8	36865	24780
84	β''_2	282.8–310.2	96.1	1178.7	44428	22140
87.9	β''_2	282.8–310.2	58.8	871.9	61459	6575
95	$\beta_0(C_{25})$	282.8–306.2	72.2	1048.2	47466	9276
97.5	$\beta_0(C_{25})$	282.8–308.2	73.0	1061.9	46239	21185
100	$\beta_0(C_{25})$	282.8–310.2	59.9	953.1	50668	12680

A dispersion of θ 1100 K (Fig. 2) is observed. The parameters N and H_E are again calculated for each composition, with an Einstein temperature equal to 1100 K. Figure 3 and Table 12 present the variations of N and H_E vs. composi-

Table 11 Calculated enthalpies and deviations from the experimental enthalpies, for the mixture containing 30 mol% $n\text{-C}_{25}$

T/K	$\Delta H_{\text{exp}}/$	$\Delta H_{\text{calc}}/$	Deviations
	J mol^{-1}		
282.8	0	-3	3
283.8	686	658	28
284.8	1308	1327	-19
285.8	1975	2004	-29
286.9	2657	2689	-32
287.9	3367	3380	-13
288.9	4079	4080	-1
289.9	4798	4786	12
290.9	5523	5500	23
291.9	6246	6221	25
292.9	6965	6950	15
294.0	7720	7687	33
295.0	8457	8431	26
296.0	9205	9182	23
297.0	9942	9941	1
298.0	10681	10708	-27
299.0	11460	11482	-22
300.0	12228	12264	-36
301.1	13014	13053	-39
302.1	13822	13850	-28
303.1	14630	14654	-24
304.1	15477	15466	11
305.2	16355	16286	69

tion. Finally, a general expression of the enthalpy $H(T,x)$ as a function of the temperature and composition is defined by the following expression:

$$H(T,x) = \frac{3R1100N(x)}{\exp\left(\frac{1100}{T}\right) - 1}$$

with: i) in the terminal solid solution ranges:

for $\beta_0(\text{C}_{23})$ and $\beta'_0(\text{C}_{23})$: $N(x) = 138.38x + 72.66$

for $\beta_0(C_{25})$ and $\beta'_0(C_{25})$: $N(x) = -49.115x + 125.32$
 where x is the molar fraction of C_{25} .

ii) for the orthorhombic intermediate solution β'' , β'_1 and β'_2 , the parameter $N(x)$:

$$N(x) = 83.5 \pm 2$$

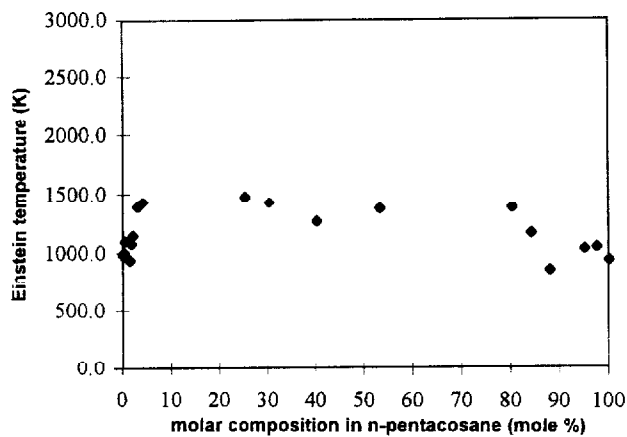


Fig. 2 Einstein temperature vs. composition

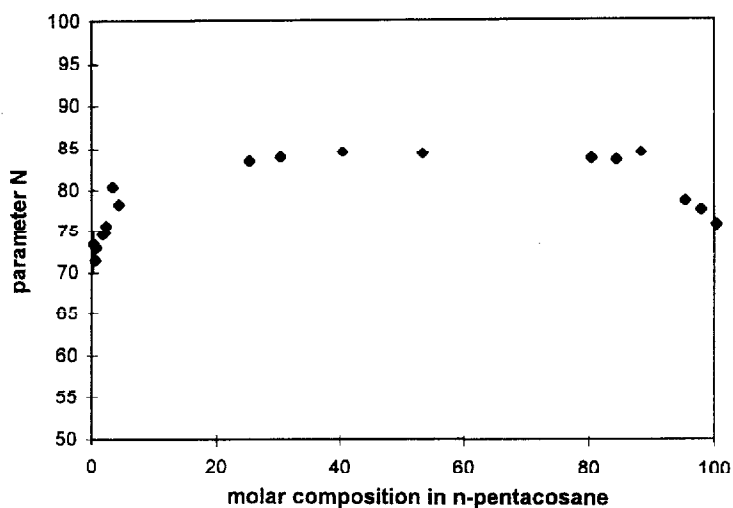


Fig. 3 Values of the parameter N vs. composition, with a constant Einstein temperature of 1100 K

Table 12 Parameters N , θ , H_E vs. composition in n -C₂₅H₅₂

$x/\text{mol}\%$ in C ₂₅ H ₅₂	Phase	Temperature domain/K	N	$\theta/$ K	$H_E/$ J mol ⁻¹	Error function/ J mol ⁻¹
0	$\beta_0(\text{C}_{23})$	282.8–307.2	73.4	1100	42002	17343
0.3	$\beta_0(\text{C}_{23})$	282.8–309.2	71.5	1100	40895	26291
0.5	$\beta_0(\text{C}_{23})$	282.8–306.2	72.9	1100	41737	20564
1.5	$\beta'_0(\text{C}_{23})$	282.8–306.2	74.5	1100	42644	44854
1.8	$\beta'_0(\text{C}_{23})$	282.8–307.1	74.7	1100	42766	17319
2	$\beta'_0(\text{C}_{23})$	282.8–305.2	75.8	1100	43389	21534
3	β_1''	282.8–308.2	80.4	1100	46150	94538
4	β_1''	282.8–307.2	78.3	1100	44921	113240
25	β_1'	282.8–305.2	83.4	1100	47848	96066
30	β_1'	282.8–305.2	83.9	1100	48177	76579
40	β_1'	282.8–306.2	84.6	1100	48453	108628
53	β_1'	282.8–307.2	84.4	1100	48371	107006
80	β_2''	282.8–308.2	83.8	1100	48077	108995
84	β_2''	282.8–310.2	83.6	1100	47947	30935
87.9	β_2''	282.8–310.2	84.6	1100	48385	67952
95	$\beta_0(\text{C}_{25})$	282.8–306.2	78.9	1100	45118	10412
97.5	$\beta_0(\text{C}_{25})$	282.8–308.2	77.8	1100	44532	22072
100	$\beta_0(\text{C}_{25})$	282.8–310.2	76.1	1100	43539	30884

Conclusions

In this work, we determined the variation of the enthalpy of C₂₃, C₂₅ and 16 binary mixtures between 282 K and 350 K. These data concerning binary mixtures of the phases $\beta_0(\text{C}_{23})$, $\beta'_0(\text{C}_{23})$, $\beta_0(\text{C}_{25})$, $\beta'_0(\text{C}_{25})$, β_1'' , β_1' , β_2'' as well as the phases of the pure n -alkanes C₂₃ and C₂₅, have been represented by an analytical expression, derived from Einstein's model of the solid state.

Expressions of the enthalpy, as a function of the temperature and molar fraction of C₂₅, has been defined for the ranges of the terminal solid solutions and of the intermediate solid solution, respectively. This study gives new results about the binary systems C₂₃:C₂₅ and these results could be used for the determination of the thermodynamic functions of mixing, necessary to calculate solid–solid equilibria.

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